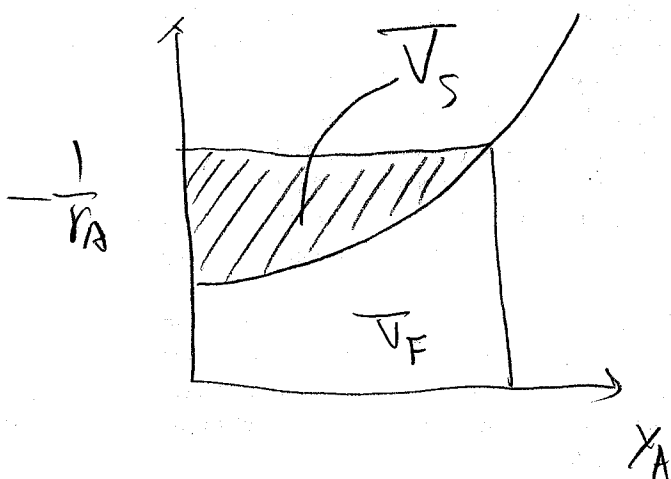


HOMEWORK #1

1. N/A

2. liquid phase reaction. there is no volume change. for CSTR

$$\begin{aligned} V &= \frac{v_0(C_{A0} - C_A)}{-r_A} = \frac{v_0(C_{A0} - C_A)}{kC_A} = \frac{v_0}{k} \left(\frac{C_{A0}}{C_A} - 1 \right) \\ &= \frac{10 \text{ dm}^3/\text{min}}{0.23 \text{ min}^{-1}} (10 - 1) \\ &= 391.3 (\text{dm}^3) \end{aligned}$$



⇒ at the same conversion volume of CSTR is V_S greater than PFR.

⇒ CSTR tends to operate at diluted situation so the average reaction rate is lower in the

reactor, so that the size must be larger to achieve the desired conversion.

3.

$$X_A = 0.9 \quad v_0 = 10 \text{ l/hr} \quad F_{A0} = 5 \text{ mol/hr}$$

$$\textcircled{1} \quad -r_A = k \quad k = 0.075 \frac{\text{mol}}{\text{hr} \cdot \text{l}}$$

$$\text{CSTR} \quad V = \frac{5 - 0.1 \cdot 5}{0.075} = 60 \text{ l} \quad \#$$

$$\text{PFR} \quad V = \frac{1}{-0.075} \int_{F_{A0}}^{F_A} dF_A = \frac{5 - 0.1 \cdot 5}{0.075} = 60 \text{ l} \quad \#$$

$$\textcircled{2} \quad -r_A = k \cdot C_A \quad k = 0.01 \text{ s}^{-1}$$

$$\text{CSTR} \quad V = \frac{5 - 0.1 \cdot 5}{3600 \cdot 0.01 \cdot \frac{5}{40}} = 0.25 \text{ l} \quad \#$$

$$\begin{aligned} \text{PFR} \quad V &= -\frac{1}{k} \int \frac{dF_A}{C_A} = -\frac{v_0}{k} \int_{C_{A0}}^{C_A} \frac{dC_A}{C_A} = \frac{v_0}{k} \ln \frac{C_{A0}}{C_A} \\ &= \frac{10}{3600 \cdot 0.01} \cdot \ln 10 = 0.64 \text{ l} \quad \# \end{aligned}$$

$$\textcircled{3} \quad -r_A = k C_A^2 \quad k = 15 \frac{\text{l}}{\text{m} \cdot \text{hr}}$$

$$\begin{aligned} \text{CSTR:} \quad V &= \frac{F_{A0} - F_A}{k \cdot C_A^2} = \frac{F_{A0} - F_A}{k \left(\frac{F_A}{v_0}\right)^2} \\ &= \frac{5 - 0.1 \cdot 5}{15 \cdot \left(\frac{0.1 \cdot 5}{10}\right)^2} = 120 \text{ l} \quad \# \end{aligned}$$

PFR:

$$\begin{aligned} V &= \frac{v_0}{k} \int_{C_{A0}}^{C_A} \frac{dC_A}{C_A^2} = \frac{v_0}{k} \left(\frac{1}{C_A} - \frac{1}{C_{A0}} \right) \\ &= \frac{10}{15} \left(\frac{10}{5 \cdot 0.1} - \frac{10}{5} \right) \\ &= 12 \text{ l} \quad \# \end{aligned}$$

4.

$$a. N_{A0} = \frac{P_T V y_{A0}}{RT} = \frac{25 \cdot 200}{0.082 \cdot 450} \cdot 0.6 = 81.3 \text{ mol} \quad \#$$

$$C_{A0} = \frac{N_{A0}}{V_0} = \frac{81.3}{200} = 0.4065 \text{ mol/l} \quad \#$$

$$b. t = \int \frac{dN_A}{r_A V} = \frac{1}{r V} \int \frac{dN_A}{C_A} = -\frac{1}{r} \int \frac{dN_A}{N_A}$$

$$= -\frac{1}{r} \ln \frac{N_A}{N_{A0}} = \frac{1}{0.015} \ln \frac{1}{0.25}$$

$$= 9.24 \text{ min} \quad \#$$

$$c. t = -\frac{V}{r} \int \frac{dN_A}{N_A^2} = \frac{V}{r} \left(\frac{1}{N_A} - \frac{1}{N_{A0}} \right)$$

$$= \frac{200}{0.95} \cdot \left(\frac{1}{81.3 \cdot 0.4} - \frac{1}{81.3} \right)$$

$$= 4.92 \text{ min} \quad \#$$

$$p = \left[(81.3 + 81.3 \cdot 0.6) \cdot 0.082 \cdot 455 \right] / 200$$

$$= 24.27 \text{ atm} \quad \#$$